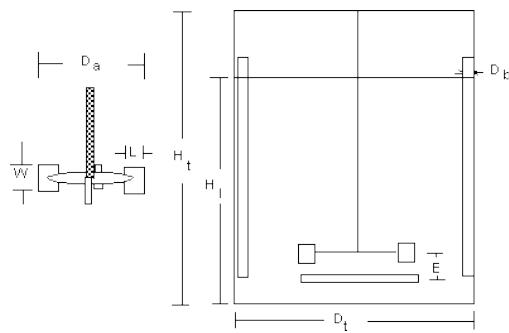


## Biochemical Engineering Exercise Session 2

### 1) Design aspects of a bioreactor



A stirred tank bioreactor is approximately cylindrical in shape. It has a total volume ( $V_t$ ) of 100,000 liters. The geometry of the reactor is defined by the following ratios:  
 $D_t:H_t=0,5$  ;  $D_a:D_t=0,33$  ;  $D_b:D_t = 0,1$

- Is it an aerated system?
- Is this type of bioreactor advantageous for mammalian cells?
- Calculate:  $D_t$ ,  $H_t$ ,  $D_a$ ,  $D_b$

## 2) Cell concentration in aerobic culture

A strain of *Azotobacter vinelandii* is cultured in a 15m<sup>3</sup> stirred Fermenter for alginate production. Under current operating conditions  $k_{LA}$  is 0.17 s<sup>-1</sup>. Oxygen solubility in the broth is approx.  $8 \times 10^{-3}$  kg m<sup>-3</sup>.

a) The specific rate of oxygen uptake is  $12.5 \text{ mmol g}^{-1} \text{ h}^{-1}$ . What is the maximum possible cell concentration?

b) The bacteria suffer growth inhibition after copper sulphate is accidentally added to the fermentation broth. This causes a reduction in oxygen uptake rate to  $3 \text{ mmol g}^{-1} \text{ h}^{-1}$ . What maximum cell concentration now be supported by the fermenter?

### 3) Specific oxygen uptake in *E. coli* culture

It is assumed that the specific oxygen uptake rate ( $q_{O_2}$ ) of *E. coli* is  $5.0 \text{ mmol g}^{-1} \text{ h}^{-1}$ .

- Which cell concentration  $X$  can be reached in a laboratory reactor with a  $k_{La}$  of  $25 \text{ h}^{-1}$  when  $C_L = 10 \% C^*$  and for the medium at  $37^\circ\text{C}$  is  $C^* = 0.17 \text{ mmol L}^{-1}$ .

### 4) Oxygen consumption

Estimate how fast the dissolved oxygen concentration is consumed in a bioreactor with  $k_{La} 1000 \text{ h}^{-1}$ , containing a  $10 \text{ g L}^{-1}$  culture growing with  $\mu = 0.5 \text{ h}^{-1}$  if the aeration is interrupted.

- Calculate the quasi-steady state oxygen concentration. Assume  $Y_{XO} = 1 \text{ g g}^{-1}$  and the oxygen solubility in the medium equilibrium with  $C^* = 7 \text{ mg L}^{-1}$ .
- In what time will the culture become completely anaerobic?

### 5) Oxygen storage capacity of fermentation broth

With a OTR (=OUR) of growing bacteria of  $1 \text{ g O}_2 (\text{L} \cdot \text{h})^{-1}$  per  $1 \text{ g L}^{-1}$  cell dry mass and approximately  $100 \text{ g L}^{-1}$  cell dry mass at the end of the growth phase, an oxygen uptake rate of  $100 \text{ g (g L)}^{-1}$  will develop. The oxygen solubility in the fermentation broth at  $28^\circ\text{C}$  is calculated at  $7.76 \text{ mg L}^{-1}$ .

a) How long will the oxygen supply last?

Note: OUR per 1 g cell dry weight =  $q_{\text{O}_2}$

### 6) Calculating saturation concentration

Calculation of the oxygen saturation concentration at different temperatures and partial oxygen pressures using the correlation of Truesdale:

T [°C]	28	37	60	28	37	60
P <sub>O<sub>2</sub></sub> [bar]	0.2121	0.2121	0.2121	1.0133	1.0133	1.0133
C* <sub>O<sub>2</sub></sub> [mg L <sup>-1</sup> ]						

### 7) Oxygen transfer in a sparged stirred tank bioreactor

Which of the following would have the highest oxygen transfer rate characteristics?

- a) A sparged stirred tank bioreactor being stirred at 200 rpm
- b) A non-sparged stirred tank bioreactor being stirred at 200 rpm
- c) A shake flask being mixed at 200 rpm
- d) All of the above would have equivalent oxygen transfer rate characteristics